

AMENDMENTS TO THE CLAIMS

This listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

1. (currently amended) A continuous contacting apparatus for separating a liquid component from a liquid mixture, the apparatus comprising:

an evaporation chamber having first and second ends, an inlet and an outlet for a carrier gas, and an inlet and an outlet for a liquid mixture, wherein the inlet for the liquid mixture and the outlet of the carrier gas are located on the first end of the evaporation chamber;

a dew-formation chamber having an inlet and an outlet for a carrier gas, and an outlet for the separable liquid component, wherein the inlet for the carrier gas of the dew-formation chamber is situated in a countercurrent manner to the inlet for the carrier gas of the evaporation chamber;

a common heat transfer wall in continuous contact with the liquid mixture, wherein the heat transfer wall is adjacent the evaporation chamber and the dew-formation chamber and is capable of providing thermal communication between the evaporation chamber and the dew-formation chamber; and

a heating apparatus for heating the carrier gas from the outlet of the evaporation chamber, wherein the heated carrier gas is directed to flow into the inlet of the dew-formation chamber[.];

wherein the apparatus provides a condensate production flux from about 0.045 to about 2.27 kg of condensate per hour/m² of heat transfer wall.

2. (previously amended) The apparatus according to claim 1 further comprising,
a feeding device for providing the liquid mixture onto the evaporation chamber side
of said heat transfer wall; and

an air mover for providing a flow of a carrier gas through the chambers, wherein the
gas flow in the evaporation chamber is countercurrent to the gas flow in the dew-formation
chamber.

3. (canceled)

4. (previously amended) The apparatus according to claim 1, further comprising a
wetting material placed on the evaporation chamber side of the heat transfer wall.

5. (previously amended) The apparatus according to claim 1, wherein the heating
apparatus is a boiler, which provides steam to the carrier gas.

6. (previously amended) The apparatus according to claim 1, wherein the heating apparatus
is a heat exchanger, wherein steam from a boiler is brought into thermal communication
with the carrier gas.

7. (previously amended) The apparatus according to claim 1, wherein the heating apparatus
is a desiccant heat exchanger, wherein a slip stream is taken from the carrier gas and reacted
with a desiccant and the heat produced by the reaction is thermally communicated to the
remainder of the carrier gas.

8. (original) The apparatus according to claim 7, wherein the desiccant is selected from
the group consisting of lithium bromide, calcium chloride, lithium chloride, and mixtures
thereof

9. (previously amended) The apparatus according to claim 1, wherein the heating apparatus is a liquid-gas contactor, wherein a reactant reacts with the carrier gas, thereby increasing the concentration of the separable liquid component in the remaining carrier gas.

10. (original) The apparatus according to claim 9, wherein the carrier gas and reactant are respectively selected from the group consisting of carbon dioxide carrier gas and potassium carbonate reactant; carbon dioxide carrier gas and monoethanol amine reactant; butane carrier gas and oil reactant; sulfur dioxide carrier gas and monoethanol amine reactant; and carbon monoxide carrier gas and copper ammonia acetate reactant.

11. (original) The apparatus according to claim 1, further comprising a plurality of spacers placed in each chamber.

12. (original) The apparatus according to claim 11, wherein the plurality of spacers are positioned to provide a serpentine-shaped channel for the carrier gas.

13. (original) The apparatus according to claim 12 further comprising airflow guides.

14. (original) The apparatus according to claim 1, wherein one or more of the chambers further comprises a filler.

15. (original) The apparatus according to claim 1, wherein the liquid mixture further comprises an anti-gellant or an anti-flocculant.

Appl. No.: 10/031,534
Amdt. Dated: January 12, 2005
Reply of Office action of August 12, 2004

Docket No. ARIZ-10542

16. (original) The apparatus according to claim 15, wherein the anti-gellant or anti-flocculant is selected from the group consisting of polyvinyl alcohol, carboxymethyl cellulose, and mixtures thereof.

17. (currently amended) A process for separating a liquid component from a liquid mixture in a continuous contacting manner, the process comprising:

- providing a heat transfer wall having an evaporation side and a dew-formation side;
- continuous contacting the liquid mixture with the evaporation side of the heat transfer wall;

- flowing a carrier gas across the evaporation side of the heat transfer wall to provide a carrier gas saturated with the separable liquid component;

- heating the saturated carrier gas; and

- flowing the heated saturated carrier gas across the dew-formation side of the heat transfer wall to provide condensation of the separable liquid component from the heated saturated carrier gas[[]] ;

- wherein the condensation of the separable liquid component is provided at a condensate production flux of from about 0.045 to about 2.27 kg of condensate per hour/m² of heat transfer wall.

18. (original) The process according to claim 17, wherein the flow of the carrier gas across the evaporation side of the heat transfer wall is countercurrent to the flow of the carrier gas across the dew-formation side of the heat transfer wall.

19. (canceled)

Appl. No.: 10/031,534
Amdt. Dated: January 12, 2005
Reply of Office action of August 12, 2004

Docket No. ARIZ-10542

20. (original) The process according to claim 17, wherein the evaporation side of the heat transfer wall further comprises a wetting material placed on the wall.

21. (original) The process according to claim 17, wherein the saturated gas is heated by a method selected from the group consisting of adding steam; gas-liquid contacting with a hot water stream; heat exchanging with a higher temperature stream; heat exchanging with a slip carrier gas stream that is brought into contact with a desiccant; and reacting the carrier gas with a reactant.

22. (original) The process according to claim 17 further comprising adding an anti-gellant or an anti-flocculant to said liquid mixture before contacting the liquid mixture with the evaporation side of the heat transfer wall.

23. (original) The process according to claim 17, wherein said anti-gellant or anti-flocculant is selected from the group consisting of polyvinyl alcohol, carboxymethyl cellulose, and mixtures thereof.